

# Januar 1992 opg 4

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Kølemiddel:  $\text{NH}_3$

Kompressor: (vandkølede kompressorcyindre)

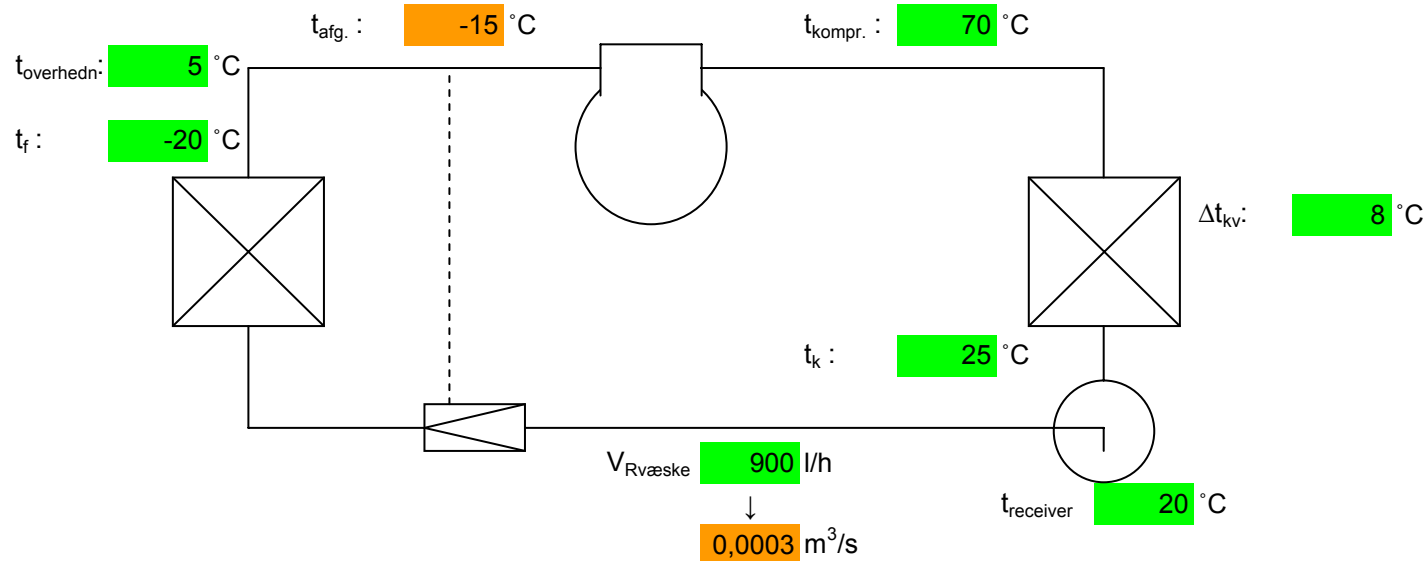
$\eta_{\text{mek}}$  0,91

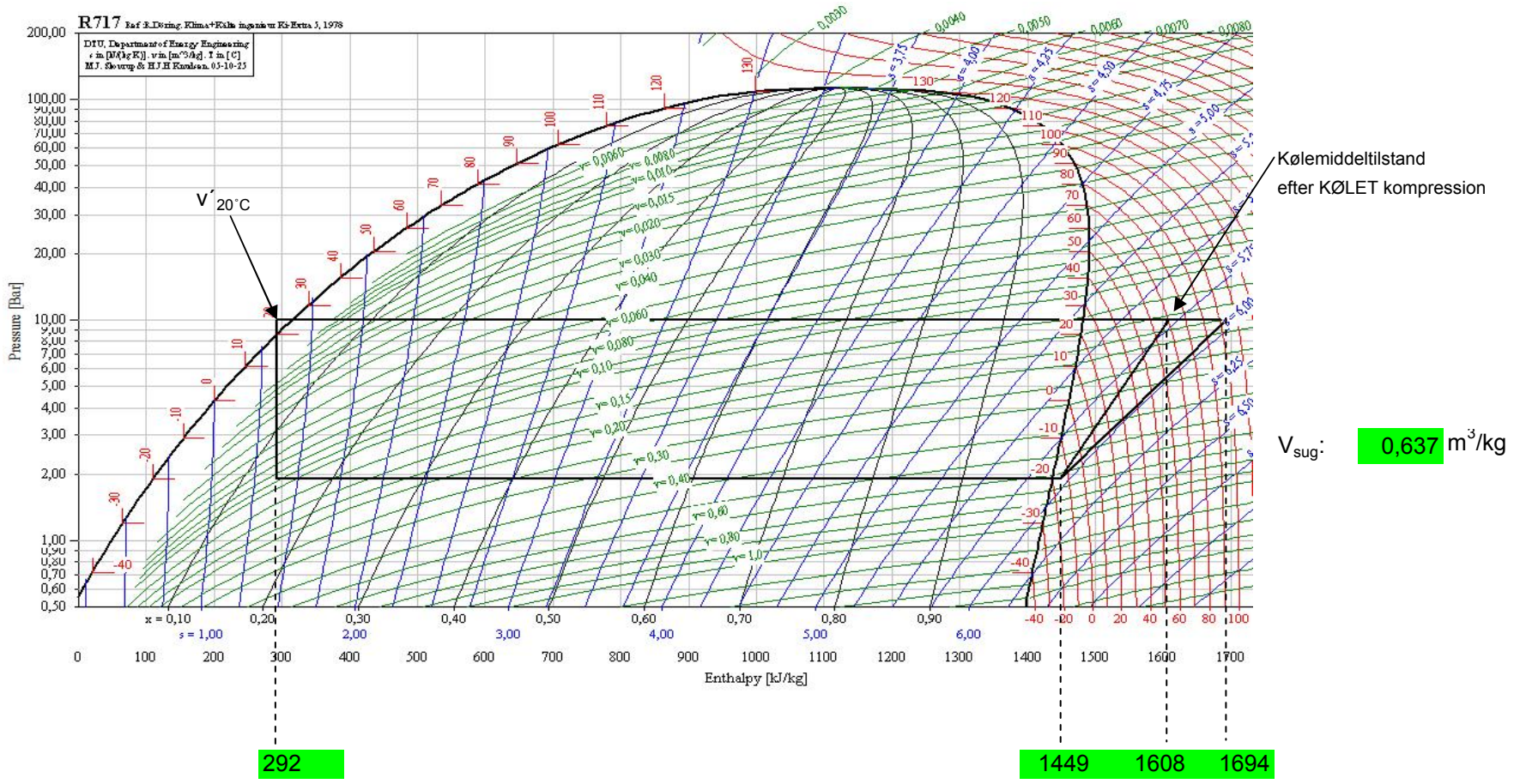
$P_{\text{tilført}}$  52 kW

$m_{\text{kv, komp}}$  2500 kg/h

→ 0,6944 kg/s

$G_{\text{kv}}$ : 4,19 kJ/kg





$\Delta h_f:$	1449	-	292	=	1156,3 kJ/kg
$\Delta h_k:$	1608	-	292	=	1315,3 kJ/kg
$\Delta h_{R\text{kom}}$	1608	-	1449	=	159 kJ/kg
$\Delta h_{\text{is}}:$	1694	-	1449	=	245,23 kJ/kg
$\Delta h_{\text{i, tab}}:$	1694	-	1608	=	86,23 kJ/kg

$v_{20^\circ\text{C}} = 1,639 \text{ l/kg}$  (tabel for væske =  $0,0016 \text{ m}^3/\text{kg}$ )

#### 4.1 Beregn anlæggets kuldeydelse, $Q_f$ , angivet i kW

$$\begin{aligned}
 P_i &= \eta_{\text{mek}} \cdot P_{\text{tilført}} = 0,91 \cdot 52 = 47,32 \text{ kW} \\
 P_{\text{tab}} &= P_{\text{tilført}} - P_i = 52 - 47,32 = 4,68 \text{ kW} \\
 m_R &= \frac{V_{\text{Rvæske}}}{V'_{20^\circ\text{C}}} = \frac{0,0003}{0,0016} = 0,1525 \text{ kg/s} \\
 Q_f &= m_R \cdot \Delta h_f = 0,1525 \cdot 1156,3 = \underline{\underline{176,38 \text{ kW}}}
 \end{aligned}$$

#### 4.2 Beregn kølevandsmængden gennem kondensatoren, angivet i kg/h

For kondensatoren gælder:

$$\begin{aligned}
 Q_k &= m_R \cdot \Delta h_k = m_{\text{kV}} \cdot c_{\text{kV}} \cdot \Delta t_{\text{kV}} \\
 m_{\text{kV, kon}} &= \frac{m_R \cdot \Delta h_k}{c_{\text{kV}} \cdot \Delta t_{\text{kV}}} = \frac{0,1525 \cdot 1315,3}{4,19 \cdot 8} = 5,99 \text{ kg/s} \\
 &= \underline{\underline{21547 \text{ kg/h}}} \text{ (kondensator)}
 \end{aligned}$$

#### 4.3 Beregn kompressorens indicerede virkningsgrad (den isentropiske virkningsgrad)

$$\begin{aligned}
 P_{\text{is}} &= m_R \cdot \Delta h_{\text{is}} = 0,1525 \cdot 245,23 = 37,40 \text{ kW} \\
 \eta_{\text{is}} &= \frac{P_{\text{is}}}{P_i} = \frac{37,40}{47,32} = \underline{\underline{0,79}}
 \end{aligned}$$

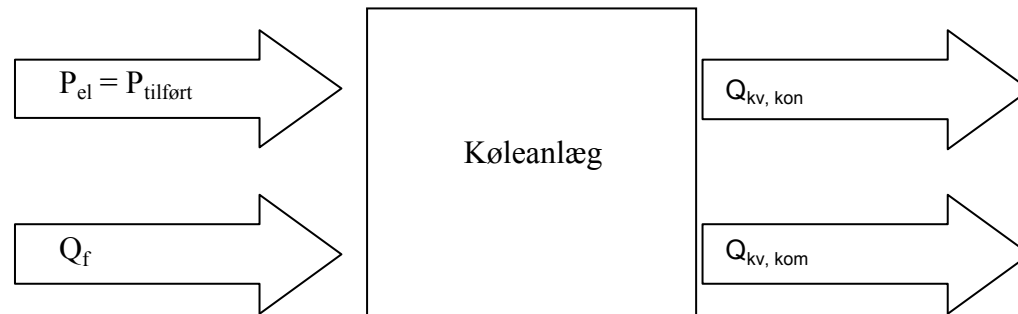
#### 4.4 Beregn kølevandets temperaturstigning gennem cylindrenes kølekapper

$$P_{\text{tilført, komp}} = Q_{R, \text{kom}} = Q_{kv, \text{kom}} = Q_{R, \text{kom}} + m_{kv, \text{kom}} \cdot c_{kv} \cdot \Delta t_{kv, \text{kom}}$$

$$Q_{R, \text{kom}} = m_R \cdot \Delta h_{R\text{kom}} = 0,1525 \cdot 159 = 24,25 \text{ kW}$$

$$\Delta t_{kv, \text{kom}} = \frac{P_{\text{tilført, kom}} - Q_{R, \text{kom}}}{m_{kv, \text{kom}} \cdot c_{kv}} = \frac{52 - 24,25}{0,6944 \cdot 4,19} = 9,5 \text{ °C}$$

#### 4.5 Opstil en varmebalance for køleanlægget



Energi tilført:			
$P_{\text{tilført}}$	=	52	kW
$Q_f$	=	176,38	kW
<hr/>			
<b>I alt</b>	=	<b>228,38</b>	<b>kW</b>

Energi bortledt:			
$Q_{kv, \text{kon}}$	=	200,63	kW
$Q_{kv, \text{kom}}$	=	27,748	kW
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<b>I alt</b>	=	<b>228,38</b>	<b>kW</b>

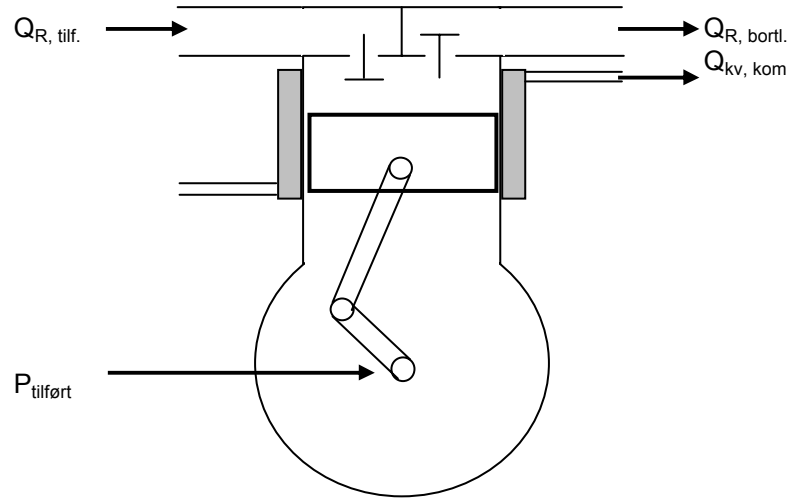
$$\sim \frac{m_{kv, \text{kon}} \cdot c_{kv} \cdot \Delta t_{kv, \text{kon}}}{5,99 \cdot 4,19 \cdot 8}$$

$$\sim \frac{m_{kv, \text{kom}} \cdot c_{kv} \cdot \Delta t_{kv, \text{kom}}}{0,69 \cdot 4,19 \cdot 9,5}$$

#### Bonus opgave

**Varmebalance for kompressor:**

Varme ind	
$Q_{R, \text{ tilf.}}$	220,94 kW
$P_{\text{ tilført}}$	52 kW
I alt ind: 272,94 kW	



Varme ud	
$Q_{R, \text{ bortl.}}$	245,20 kW
$Q_{kv, \text{ kom}}$	27,748 kW
I alt ud: 272,94 kW	

$$Q_{R, \text{ tilf.}} = m_R \cdot h_{\text{tilgang}} = 0,1525 \cdot 1449 = 220,94 \text{ kW}$$

$$Q_{R, \text{ bortl.}} = m_R \cdot h_{\text{afgang}} = 0,1525 \cdot 1608 = 245,20 \text{ kW}$$